



# AN APPLICATION OF RISK- BASED DESIGN CRITERIA

Stephen D. Unwin

Unwin Company, Columbus , Ohio

&

Robert R. Roberts

Roberts & Roberts, San Diego, California

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# OUTLINE

- Background/Objectives
- Methods
- Results
- Conclusions

# BACKGROUND

- HF Alkylation Unit operated by Ultramar Refining in Wilmington, CA
- Decision to install an (acid) Automatic Isolation and Evacuation System (AIES)
- Proposed local regulation in place specifying AIES design (based on API RP-751)
- Several design/operational options available

# RISK-BASED DESIGN SELECTION

- Operational risk/reliability identified by Ultramar as key design selection criterion
  - Study commissioned
- Study objectives:
  - Quantify accident risks associated with each of three AIES design options
  - Identify and understand design features that *drive* risk profiles
  - Develop robust basis for selection among designs

# OPTIONAL DESIGN CONCEPTS

- Option 1:
  - Emergency acid receiving vessel located outside battery limits
  - Given acid release, leak location diagnosed and acid transferred to receiving vessel
- Option 2:
  - Unit reconfigured from Series Recycle (SRC) to Series Acid Configuration (SAC)

# OPTIONAL DESIGN CONCEPTS - Contd.

- Option 2 (Contd.):
  - Given acid release, all major acid holding vessels isolated. If release persists, leak location diagnosed and acid transferred to intact settler
- Option 3:
  - Combination of previous options:
    - Unit converted to SAC design
    - Given release, acid evacuated to remote receiving vessel

# RISK METHODS

- Integrated Risk Model:
  - Front End: Model potential causes, locations, sizes, and likelihoods of acid releases from system
  - Analysis of system capabilities: identify those releases that are mitigatable by each AIES design option
    - Successful mitigation: release less than 1,500 gallons
    - Consideration of diagnosis and response times

# RISK METHODS - Contd.

- Back End: Model potential failure modes of each AIES system design, and estimate failure likelihoods
- Analysis of system reliabilities
  - reliability block diagram analysis
  - systematic identification of failure modes: human errors, equipment failures, support system failures
- Analysis of consequences of unmitigatable or unmitigated releases:
  - Release size used as surrogate consequence measure



# UNDERLYING RISK FORMULA

- $R = \Sigma (I_m \times A_{mn} \times C_m) + \Sigma (J_i \times D_i)$
- $R$  = Risk metric
- $I_m$  = Annual probability of mitigatable leak at location/size  $m$
- $J_i$  = Annual probability of unmitigatable leak at location/size  $i$
- $A_{mn}$  = Probability of AIES failure via mode  $n$  given leak  $m$
- $C_m/D_i$  = Consequence severity of leak  $m/i$

# AIES FAILURE MODES: EXAMPLE CUT-SETS

AIES OPTION: 3  
 RESPONSE MODE FOR: RELEASE IN ACID STORAGE SECTION  
 TOTAL FAILURE PROBABILITY = 1.21E-01

<u>CUT-SET</u>	<u>DESCRIPTION</u>	<u>BE PROB<sup>a</sup></u>	<u>CS PROB<sup>b</sup></u>
1 PEVAC-STFL	Evac Pump PEVAC Fails to Start from Cold and Evac Acid from Storage Section	6.46E-02	6.46E-02
2 H-DET-HFOK-OP1/3	Operators Fails to Detect Release Given HF Detector Alarm	3.67E-02	3.67E-02
3 HF-DET-FL	HF Detectors Fail to Respond to Release	1.98E-01	9.41E-03
H-DET-HFFL-OP1/3	Operators Fail to Detect Release Given HF Detector Failure	4.75E-02	
4 MOV-J-FC	MOV J Fails Closed	5.09E-03	5.09E-03
5 MOV-K-FC	MOV K Fails Closed	5.09E-03	5.09E-03
6 H-MOV-DIS	Failure to Reconnect MOV Power After PLC Logic Test	3.00E-03	3.00E-03
7 H-XFER-OP1/3	Operator Fails to Diagnose Release Location and Initiate Evacuation	2.67E-03	2.67E-03

a Probability of basic event given demand on AIES

b Probability of cut-set (= product of constituent basic event probabilities) given demand on AIES

# AIES RELIABILITY

<b>AIES RESPONSE MODES</b>			
<b>AIES OPTION</b>	<b>MODE</b>	<b>RELEASE SITE</b>	<b>UNAVAILABILITY<sup>a</sup></b>
<b>OPTION 1</b>	1	Acid Storage Section	1.21E-1
	2	Reactor No. 1 Section	7.09E-2
	3	Reactor No. 2 Section	7.09E-2
	4	Acid Settler No. 1 Section	7.56E-2
	5	Acid Settler No. 2 Section	7.56E-2
<b>OPTION 2</b>	1	Line or Reactor Vessel	2.85E-2
	2	Acid Circulation Pump	9.54E-3
	3	Acid Storage Vessel	1.03E-1
	4	An Acid Settler Vessel	6.66E-2
<b>OPTION 3</b>	1	Acid Storage Section	1.21E-1
	2	Reactor No. 1 Section	7.09E-2
	3	Reactor No. 2 Section	7.09E-2
	4	Acid Settler No. 1 Section	6.62E-2
	5	Acid Settler No. 2 Section	6.62E-2

a Probability of AIES failure given the event of a mitigatable release

# RISK ESTIMATES

<b>AIES RISK COMPARISONS</b>			
<b>RISK PARAMETER</b> (Annual)	<b>AIES OPTION</b>		
	Option 1	Option 2	Option 3
Release (IE) Frequency	<b>1.8E-1</b>	<b>9.2E-2</b>	<b>9.2E-2</b>
Unmitigatable Release Frequency	<b>6.6E-4</b>	<b>4.4E-4</b>	<b>4.8E-4</b>
Unmitigated Release Frequency	<b>1.4E-2</b>	<b>1.6E-3</b>	<b>6.6E-3</b>
AIES Unavailability	<b>7.6E-2</b>	<b>1.2E-2</b>	<b>6.7E-2</b>
Risk	<b>1.5</b>	<b>0.51</b>	<b>0.87</b>

# RISK DRIVERS

- SAC (Options 2 and 3) have lower leak probability
  - Single active pump
  - Fewer potential leak sites
- Leak isolation (Option 2) more reliable than acid evaluation
  - Isolation less reliant on leak location diagnosis
  - Greater hardware reliability for isolation
  - Need to transfer acid is unlikely

# CONCLUSIONS

- Acid isolation/transfer design selected in preference to acid evacuation design
- Risk-based case for AIES design selection accepted by regulatory agency
- Unit now operational with AIES in place